World Journal of Engineering Research and Technology



WJERT

www.wjert.org

Impact Factor Value: 5.924



MODELLING THE DRYING KINETICS OF RED CHILIES AS A FUNCTION OF LAYER THICKNESS

M. M. M. Najla¹ and R. Bawatharani^{*2}

Department of Agricultural Engineering, Faculty of Agriculture, Eastern University, Sri

Lanka.

Article Revised on 26/02/2021

Article Accepted on 16/03/2021

*Corresponding Author

Article Received on 06/02/2021

R. Bawatharani Department of Agricultural Engineering, Faculty of Agriculture, Eastern University, Sri Lanka.

ABSTRACT

Modelling the drying kinetics of red chilies (Capsicum annuum L) were studied as thin layer with sample thicknesses of 1, 2 and 3 cm in a natural convective solar dryer. Red chilies were dried from an initial moisture content of about 81.23% (w.b) to a moisture content of 7.13% (w.b). The drying data were fitted with two thin layer drying models

namely Page model and Henderson-Pabis model. The values of the empirical parameters for the models were determined by the regression equation of the best fitted line. The fit of goodness of the models were evaluated by using correlation coefficient (r), Chi-square (χ^2) and Root Mean Square Error (RMSE). Both models satisfactorily described the drying curve of chilies at 1cm layer thickness. In comparing the experimental moisture values with those model predicted values, it was shown that the Henderson-Pabis model displayed the best fit quality with correlation coefficient of 0.85, χ^2 of 0.0213 and RMSE of 0.128 concluding that Henderson-Pabis model is optimal for simulating drying kinetics of red chilies at 1cm layer thickness.

KEYWORDS: Chi-square, Convective solar dryer, Henderson-Pabis model, Page model, Root Mean Square Error.

INTRODUCTION

Chilli is one of the important spices in Sri Lankan meals. It is mainly grown for dry chilli production with an annual production of 7,500 Mt (Central Bank Report, 2002). However, it is harvested as green pods as well. The red chilies contain a moisture content in the range of

300%-400% (db) at the time of harvest which is prone to pest attack during storage (Chand and Singh, 2007). Thus, reducing the moisture content to 8-9% (db) is recommended for ideal processing and storage conditions which is achieved by means of drying (Chand and Singh, 2007).

Drying is a complex thermo-physical and biochemical process with simultaneous heat and mass transfer between the surface of the material and the surrounding media (Hossain and Bala 2002). Modelling drying kinetics has proved to be an important tool used to analyze these transfer processes of agricultural products during drying. Thin-layer drying equations are often used to describe the drying kinetics of various types of agricultural produces. Thus, numerous mathematical models for the thin layer drying of many agricultural products have been proposed.

These models fall mainly into three categories, namely, theoretical, semi-theoretical and empirical. However, the empirical equations are easily applied to drying simulation as they depend on experimental data. The empirical models derive a direct relationship between the average moisture content and drying time (Keey,1972). The present study was therefore, undertaken to model the thin layer drying characteristics of red chilies with different layer thicknesses in a natural convective solar dryer. The objective of this study was to model the drying kinetics of red chilies using two thin layer drying models namely '*Page*' and '*Henderson and Pabis*' model.

MATERIALS AND METHODS

Sample preparation

Freshly harvested red chilli samples were cleaned and stored in a refrigerator at 4° C until the drying experiments. Before the experiments, the samples were removed from the refrigerator and their temperature were allowed to become equilibrium with that of atmospheric temperature ($27 \pm 1^{\circ}$ C).

Drying experiment

Drying treatments were performed in a natural convection solar dryer between 8.00 a.m - 4.00 p.m on bright sunny days. Approximately 1kg of chili samples with initial moisture content of 90.3% were uniformly spread on stainless steel rays and kept inside the dryer. Drying was carried out at 1cm, 2cm and 3cm layer thicknesses in separate trays. The drying runs were continued until an equilibrium moisture content of 7.13% (wb) was obtained. The

weights of the samples were taken using an electronic balance at 3-hour interval until the weight was constant (samples attained equilibrium moisture content with the drying air conditions). The weight of the samples was taken quickly to avoid interference with the drying process. It was assumed that both moisture content and temperature of samples were uniform throughout the layers at any given time during the drying process. Around 5g of sample from each replication were taken to find out the moisture content. The final moisture content of the samples was determined by the oven drying method and the value obtained was taken as the equilibrium moisture content of the sample (at the drying air conditions). Each drying layer thicknesses were replicated thrice and the mean values were used for data analysis.

Thin layer drying models

Two thin layer drying models were used to describe the drying characteristics of chilies and to determine the model parameters by fitting experimental data. The thin layer drying models used in this study are given in Table 1.

Table 1: Thin lay	yer drying m	odels applied	to the drying	of red chilies.
-------------------	--------------	---------------	---------------	-----------------

No	Model Name	Model Equation	Reference
1.	Page	$MR = exp(-kt^n)$	Page, 1949
2.	Henderson and Pabis	$MR = a \ exp \ (-kt)$	Henderson and Pabis, 1961

Evaluation of models

Based on the initial moisture content from oven drying, the weight loss was measured in order to calculate the moisture ratio. The moisture ratio of chillies at a given time, t was calculated as reported by Goyal *et al.* (2006) and Akoy (2014). The drying curve for each experiment was obtained by plotting the dimensionless moisture ratio of the sample vs. the drying time.

$$MR = \frac{M_t - M_e}{M_i - M_e} \dots Equation 1$$

Where,

MR is moisture ratio

 M_i and M_e are the initial and equilibrium dry basis moisture contents, %

 M_t is dry basis moisture content at any time 't'

Najla and Bawatharani.

Determination of drying constants

The two thin-layer drying models were transformed for the determination of the constants as follows:

1. Page Model

 $MR = exp(-kt^n)$ Equation 2

 $\ln MR = -kt^{n} - \ln(MR) = kt^{n}$ $\ln (-ln(MR)) = \ln k + n lnt$ $MR = \ln k + n. lnt \qquad \text{Equation 3}$

Equation 3 is in the form of a straight line. The relationship is as follows:

y = MRm = n $x = \ln t$ $c = \ln k$

Where, MR is the moisture ratio, 't' is time (hour), and 'k' (h^{-1}) and 'n' are empirical parameters of the model.

2. Henderson - Pabis Model

 $MR = a.\exp(-kt)..$ Equation 4 ln $MR = \ln a - kt$ ln $MR = -kt + \ln a$ Equation 5 y = -m. x + C

The equation above is also in the form of a straight line and they relate as follows:

 $y = \ln MR$ m = -kx = t and $c = \ln a$

Where,

MR is the moisture ratio, 't' is time (hour), and 'a', 'k' and 'n' are empirical parameters of the model.

www.wjert.org

The experimental data were fitted in the straight line form of *Page* model and *Henderson-Pabis* model against changes in moisture ratio versus natural log of drying time. The model empirical parameters (drying constants) were determined by the regression equation of the best fitted line.

Fitness of the models

Page model and *Henderson & Pabis* model were fitted with the drying data to predict the moisture ratio (MR). The correlation coefficient (*r*) was used as primary criteria for selecting the model that best fit the experimental data. In addition to this, the models were also evaluated based on the Chi-square (χ^2) and the Root Mean Square Error (RMSE). The lower chi-square (χ^2) and RMSE values and the higher correlation coefficient values were chosen as the basis for goodness of fit (Akpinar *et al.*, 2006; Akpinar et al., 2003a, b, c; Günhan et al., 2005; Midilli and Kucuk, 2003).

$$r = \frac{\sum_{i=1}^{N} (MR_{pre,i} - MR_{exp,avg})^{2}}{\sum_{i=1}^{N} (MR_{exp,i} - MR_{exp,avg})^{2}} \dots Equation 6$$

$$\chi^{2} = \frac{\sum_{i=1}^{n} (MR_{exp,i} - MR_{pre,i})^{2}}{N-n} \dots Equation 7$$

$$RMSE = \sqrt{\frac{\sum_{i=1}^{N} (MR_{exp,i} - MR_{pre,i})^{2}}{N}} \dots Equation 8$$

Where,

MRexp,*i* - *i*th experimentally observed moisture ratio,

MRpre,*i* - *i*th predicted moisture ratio,

MRpre, avg - average experimental moisture ratio,

N - Number of observations

n - Number constants.

RESULTS AND DISCUSSION

Determination of empirical parameters of the models

The estimated empirical parameters of the two models for all the three drying layer thicknesses are presented in Table 2. The estimated value of the drying rate constant (k) decreased with the increase in layer thickness in both models. This implies that with increase in layer thickness, drying curve becomes less steep indicating decrease in drying rate.

Layer thickness	Page 'n'	Page ' k'	Henderson-Pabis 'a'	Henderson-Pabis 'k'
1 cm	-0.2736	8.3178	1.2248	-0.0531
2 cm	-0.1664	7.1771	1.1768	-0.0183
3 cm	-0.1095	5.2941	1.0731	-0.0069

 Table 2: Empirical parameters of the fitted drying models.

Fitting the thin layer drying models to the drying curves

The accuracy of both models were evaluated by comparing the predicted moisture ratios with the observed values as shown in Figures 1-6 for varied thicknesses. For each investigated layer thickness, the experimental drying data were fitted in the Henderson–Pabis model and Page model. Figures 1-6 present the variation of moisture ratio as a function of drying layer thickness. It was observed that when moisture ratio decreased with time, the difference between moisture ratios increased gradually from beginning to end of drying. Both models provided a good conformity between the experimental data and the predicted moisture ratios of different layers of chilies dried in the natural convective solar dryer.



Figure 1: Comparison of experimental and predicted moisture ratio values by *Page* model at 1cm layer thickness.



Figure 2: Comparison of experimental and predicted moisture ratio values by *Page* model at 2cm layer thickness.

www.wjert.org







Figure 4: Comparison of experimental and predicted moisture ratio values by *Henderson-Pabis* model at 1cm layer thickness.



Figure 5: Comparison of experimental and predicted moisture ratio values by *Henderson-Pabis* model at 2cm layer thickness.



Figure 6: Comparison of experimental and predicted moisture ratio values by *Henderson-Pabis* model at 3cm layer thickness.

```
www.wjert.org
```

Goodness of the fit of models

The accuracy of both models was evaluated by comparing the predicted moisture ratios with the observed values. The summary of statistical evaluation of both models using three different criteria are presented in the Tables 3 as per the procedure described by Akpinar *et al.* (2006).

	Drying model	Layer thickness of chilies	χ^2	r	RMSE
Page	Page	1cm	0.022	0.81	0.132
		2cm	1.178	0.38	1.019
		3cm	0.059	0.5	0.232
		1cm	0.021	0.84	0.128
	Henderson and Pabis	2cm	1.084	0.43	0.978
		3cm	0.048	0.48	0.211

 χ^2 = Chi square, r = Correlation coefficient, RMSE = Root-Mean-Square Error

Henderson & Pabis model displayed correlation coefficient (*r*) range from 0.43 to 0.85 and RMSE varied from 0.128 to 0.978 cross the three drying layers of chilies. It also produced Chi-square (χ^2) values from 0.0213 to 1.084. However, *r* values varied from 0.38 to 0.81 and the χ^2 varied from 0.022 - 1.178 and RMSE varied from 0.132 - 1.019 for *Page* model across the three drying layers of chilies.

Both Page model and Henderson-Pabis model gave consistently high correlation coefficient values of 0.81 and 0.85 respectively at 1cm layer thickness, indicating that both models can satisfactorily describe the drying behavior of chilies with layer thickness of 1cm. Both models did not display acceptable correlation coefficient and RMSE at 2cm and 3cm layer thicknesses. Therefore, both models show best fit only with the layer thickness of 1cm. This could be because that both models being empirical, they are capable of describing thin layer water removal and the heat penetration during drying (Da Silva *et al.*, 2014). As a consequence, the model fitness was found to be poor at 2cm and 3cm layer thicknesses.

However, studies show that *Page* model was also reported to fit the thin layer drying data better than other models in many earlier studies such as Akpinar *et al.* (2006) for aromatic plants, Doymaz (2004) for carrots and Hossain and Bala (2002) for green chillies. The *Page* model has been reported to exhibit a better fit than other models in accurately simulating the drying curves of chili (Tunde-Akintunde, 2011), (Doymaz and Pala, 2002) rape seed (Han *et al.*, 2011.), okra, (Simal *et al.*, 2005) and kiwi. *Henderson & Pabis* model was also

successfully used by (Doymaz, 2004; Sacilik *et al.*, 2006) for the prediction of drying time and for generalization of drying curves. However, in this present study it was observed that *Henderson - Pabis* model produced the highest *r* values and the lowest χ^2 , RMSE values than *Page* model at all the three layer thicknesses evaluated.

Drying of materials having high moisture content is a complicated process involving simultaneous heat and mass transfer (Yilbas *et al.*, 2003). Therefore, the thin-layer drying models used in this study describe the process of drying in a single layer of chilies. Because layer thicknesses maintain its moisture because of low air movement within masses of chillies that may require longer time to dry. As drying depth increased, there was a linear increase in drying time and vice versa. As these models consider only the external resistance to moisture transfer between product and drying air (Midilli *et al.*, 2002, Panchariya *et al.*, 2002) they neglect the fundamentals of drying process and presents a direct relationship between average moisture and drying (Ozdemir and Devres 1999, Wang and Singh 1978). Hence, the goodness of the fit of these models at 2cm and 3cm of drying layer thickness were found to be unsatisfactory.

Both models exhibited *r* values more than 0.8 at 1cm layer thickness, suggesting that the selected models gave excellent fit to the experimental data Though, both models were comparable with each other in terms of modeling accuracy (Table 3), *Henderson-Pabis* model may be assumed to represent the thin layer drying of red chilies better in a natural convective solar dryer.

CONCLUSIONS

Model fitting procedure shows that both *Page* model and *Henderson-Pabis* model showed the best curve fitting for the experimental moisture ratio value for the chillies with 1cm layer thickness in a natural convective solar dryer. Both models did not show better fit with 2 cm and 3 cm layer thicknesses. *Henderson & Pabis* model was found to be better than *Page* model due to its highest r (0.85) and lower values of χ^2 (0.0213) and RMSE (0.128). Therefore, it can be concluded that *Henderson-Pabis* model better described the drying curves of chili in natural convective solar-dryer with 1cm layer thickness.

ACKNOWLEDGEMENT

The authors wish to acknowledge the technical support provided by Mr.T.Sritharan during the drying experiment.

REFERENCES

- 1. Akoy, E. O. M. Effect of drying temperature on some quality attributes of mango slices. *International Journal of Innovation and Scientific Research*, 2014; 4(2): 91-99.
- 2. Akpinar, E. K. Determination of suitable thin layer drying curve model for some vegetables and fruits. *Journal of Food Engineering*, 2006; 73(1): 75- 84.
- Akpinar, E., Midilli, A., & Bicer, Y. Single layer drying behaviour of potato slices in a convective cyclone dryer and mathematical modelling. *Energy conversion and management*, 2003; 44(10): 1689-1705.
- 4. Akpinar, E.K., Bicer, Y. and Yildiz, C. Thin layer drying of red pepper. *Journal of Food Engineering*, 2003; 55: 99–104.
- 5. Annual report Central Bank of Sri Lanka, 2002.
- 6. Chand, T. and Singh, J. Effect of different physical and chemical treatments on drying behaviour of red chilli. *J. Res.*, 2007; 44: 138-44.
- Da Silva, W. P., Silva, C. M., Gama, F. J., & Gomes, J. P. Mathematical models to describe thin-layer drying and to determine drying rate of whole bananas. *Journal of the Saudi Society of Agricultural Sciences*, 2014; 13(1): 67-74.
- 8. Doymaz, I. Convective air-drying characteristics of thin layer carrots. *Journal of Food Engineering*, 2004; 61(3): 359-364.
- Doymaz, I., & Pala, M. Hot-air drying characteristics of red pepper. Journal of Food Engineering, 2002; 55(4): 331-335.
- Goyal, R. K., Kingsly, A. R. P., Manikantan, M. R., & Ilyas, S. M. Thin- layer drying kinetics of raw mango slices. *Biosystems Engineering*, 2006; 95(1): 43-49.
- 11. Gunhan, T., Demir, V., Hancioglu, E., & Hepbasli, A. Mathematical modelling of drying of bay leaves. *Energy Conversion and Management*, 2005; 46(11): 1667-1679.
- Han, J. W., & Keum, D. H. Thin layer drying characteristics of rapeseed (Brassica napus L.). *Journal of Stored Products Research*, 2011; 47(1): 32-38.
- 13. Henderson, S. M., & Pabis, S. Grain drying theory I: Temperature effect on drying coefficient. *Journal of Agricultural Research Engineering*, 1961; 6: 169-174.
- Hossain, M. A., & Bala, B. K. Thin-layer drying characteristics for green chilli. *Drying Technology*, 2002; 20(2): 489-505.
- 15. Keey, R. B. Drying: principles and practice. New York: Pergoman Press., 1972.
- Midilli, A., Kucuk, H. and Yapar, Z.A. New model for single layer drying. Drying Technol, 2002; 20(7): 1503–1513.

- 17. Midilli, A., and Kucuk, H. Mathematical modeling of thin layer drying of pistachio by using solar energy. *Energy conversion and Management*, 2003; 44(7): 1111-1122.
- 18. Ozdemir, M. and Devres, Y.O. The thin layer drying characteristics of hazelnuts during roasting. *Journal of food Engineering*, 1999; 42: 225–233.
- 19. Page, G. E. Factors influencing the maximum rates of air drying shelled corn in thin layers. Unpublished M.S. thesis, Purdue University, West Lafayette, Ind., 1949.
- 20. Panchariya, P.C., Popovic, D. and Sharma, A.L. Thin-layer modelling of black tea drying process. *Journal of food Engineering*, 2002; 52: 349–357.
- 21. Sacilik, K., Keskin, R., & Elicin, A. K. Mathematical modelling of solar tunnel drying of thin layer organic tomato. *Journal of food Engineering*, 2006; 73(3): 231-238.
- 22. Simal, S., Femenia, A., Garau, M. C., & Rosselló, C. Use of exponential, Page's and diffusional models to simulate the drying kinetics of kiwi fruit. *Journal of Food Engineering*, 2005; 66(3): 323-328.
- 23. Tunde-Akintunde, T. Y. Mathematical modeling of sun and solar drying of chilli pepper. *Renewable Energy*, 2011; 36(8): 2139-2145.
- 24. Wang, C.Y. and Singh, R.P. Use of variable equilibrium moisture content in modelling rice drying. *Trans Am Soc Agric Eng.*, 1978; 11: 668–672.
- 25. Yilbas, B.S., Hussain, M.M. and Dincer, I. Heat and moisture diffusion in slab products to convective boundary condition. *Heat Mass Transf*, 2003; 39: 471–476.